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85-265177/43 LAB LAFON L	A96 B07	LAFO 30.03.84 *EP -159-237-A	A(12-VI) B(4-B1B, 11-C5, 12-M11)
30.03.84-FR-005058 (23.10.85) A61k-9/10 Pharmaceutical oral dosage forms - produced by freeze drying lipid-water emulsion C85-114655 E(AT BE CH DE FR GB IT LI LU NL SE)			ive ingredient during mfr. than conventional tablets, integrate rapidly in aq. media, and give higher blood of active ingredient than conventional tablets.
Prodn. of oral dosage forms contg. at least one pharmaceut- ically active ingredient is effected by: (a) preparing a liq. lipid phase by stirring at 80°C or less to mix all the lipid phase components; (b) preparing an aq. phase contg. one or more organic fillers and/or thickening agents, by stirring at 80°C or less to mix the water and other aq. phase components; (c) adding the lipid phase to the aq. phase while stirring at 10-80°C to form a homogeneous emulsion; (d) distributing the emulsion in cellular packs; and (e) freeze drying the emulsion by cooling to -20 to -50°C. and applying a vacuum of 0.13-80 Pa. The active ingredient is added before step (d).			PREFERRED MATERIALS Fillers are lactose, whole milk powder, skim-milk glycine, mannitol and/or maltodextrins. Thickeners are natural or synthetic gums, cellulose derivs., pectin, bentonite, colloidal silica, polyvinyl polyvinylpyrrolidone and/or acrylic (co)polymers.
ADVANTAGE The process produces tablets which are easier to handle than liq. emulsions, are less subject to decompn. of the act-			PREFERRED CONDITIONS The aq. phase contains 10-85 (esp. 15-65) wt. % fi and thickener. The wt. ratio of lipid phase to aq. ph is 1 : 4-100, esp. 1 : 6-50. The active ingredient is to the emulsion at -1 to -5°C. A surfactant is added to the lipid or aq. phase in of 0.2-10 (esp. 0.4-8) wt. % based on the total emulsion. EXAMPLE A mixt. of 200 pts. wt. caprylic/capric acid trigly 20 pts. wt. polysorbate 60 and 20 pts. wt. ethoxylated acid glycerides was added at 65°C to a soln. of 10 pt. EP-1592

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(54) Galenic form for oral administration and its method of preparation by lyophilization of an oil-in-water emulsion.

(57) This invention is concerned with a method for preparing a novel porous galenic form by lyophilization of an oil-in-water emulsion containing at least one pharmaceutically active ingredient, which comprises the following steps:

a) preparation of the lipid phase by stirring at a temperature lower than or equal to 80°C so as to mix all the lipid-phase components, the lipid phase thus prepared being in the liquid state;

b) preparation of the aqueous phase, which comprises at least one substance selected from the group consisting of organic fillers and thickening agents, by stirring at a temperature lower than or equal to 80°C so as to mix the water and the other components of the aqueous phase;

c) preparation of an emulsion under stirring at a temperature within the range of 10°C to 80°C by introducing the liquid lipid phase into the aqueous phase so as to ensure that the resulting emulsion is homogeneous ;

d) distribution of the resulting mixture into alveolar packs ;

e) freezing of the contents of the alveolar packs at a temperature within the range of -20°C to -50°C followed by lyophilization of said contents under a pressure within the range of approximately 80 Pa to approximately 0.13 Pa with a heat supply such that the temperature of the treated mass is always lower than the initial melting temperature of said mass ;

the pharmaceutically active substance being introduced prior to step d), if necessary by fractions.

The invention also relates to the galenic form obtained in accordance with this method and constituting a novel industrial product.

EP 0 159 237 A1

GALENIC FORM FOR ORAL ADMINISTRATION AND ITS METHOD OF
PREPARATION BY LYOPHILIZATION OF AN OIL-IN-WATER EMULSION.

The present invention relates to an industrial product consisting of a novel galenic form for oral administration of the solid oral emulsion type. The invention is mainly concerned with the method of preparation of this novel galenic form by lyophilization of an emulsion of the oil-in-water type.

It is known that emulsions constitute a liquid galenic form which is of interest in the biopharmaceutical field for oral administration. It is in fact possible in an emulsion system to introduce a wide range of substances, especially auxiliary substances such as fat-absorbent products, surface-active products, solubilizing agents, solvents, and so on, which provide a certain number of advantages, namely as follows :

- 15 - modification of the absorption of medicinal drugs :
 - . either in order to achieve enhanced bioavailability,
 - . or to defer the release of active ingredients ;
- protection of the labile or fragile active ingredients which are liable to be degraded by an unfavorable pH medium or by enzymes of the digestive tract ;
- 20 - improvement by means of suitable adjuvants, in the tolerance of certain aggressive active ingredients (for example the anti-inflammatory agents and certain

antibiotics) with respect to the mucous membranes of the digestive system.

However, this liquid galenic form is out of date since it gives rise in the first place to a certain number of technical problems :

- it is limited to stable active ingredients, especially in the aqueous phase ;
- it is not applicable to associations of substances which are incompatible with each other in the aqueous phase ;
- 10 - for the preservation of an emulsion of this type, its formulation essentially requires the presence of a certain number of preserving agents which are not always conducive to tolerance ;
- the emulsions are heat-sensitive and entail the need for
- 15 storage precautions.

In the second place, the practical utilization of the liquid galenic form is subject to a certain number of disadvantages arising from the presentation (a liquid packaged in a vial or bottle is not always convenient in

20 ambulatory treatment), from the time limit allowed for use (once it has been opened, the vial must be used within a period of one to several weeks) and from the fact that dosing of the active ingredients is a random process, even when using dose spoons.

25 The present invention proposes a novel technical solution which involves lyophilization of an emulsion of

the oil-in-water type in order to overcome the disadvantages of liquid emulsions while retaining their advantages.

The essential advantage of the solid emulsions in accordance with the invention over compressed tablets

5 lies in the fact that the active ingredients are maintained in the state in which they are used in practice whereas, in the tablets, said active ingredients are liable to undergo extensive changes during the manufacturing process. For example, micronization which is often

10 necessary for the purpose of improving the bioavailability of sparingly soluble products is attended by problems of wettability and reagglomeration by electrostatic phenomena. These phenomena are more marked in the case of the sub-

15 micronic products which are obtained by various techniques such as nebulization, for example, and prove difficult and even impossible to recover by the usual methods. The present invention provides the only method for obtaining a solid form containing particles in such a finely divided state. In fact, in accordance with the invention, these

20 disadvantages are overcome by utilizing a suspension which is perfectly dispersed and deflocculated by means of suitable adjuvants. As a result of lyophilization, this suspension is "frozen" and its properties are completely restored at the moment of utilization of the solid form

25 in accordance with the invention. The manufacture of tablets does not make it possible to retain said

properties either directly or indirectly by addition of
correcting means since the quantities of water and/or
adjuvants which it is possible to employ are rarely
sufficient to produce a dispersion of particles throughout
5 the entire mass. In addition, the manufacture of tablets
entails the use of other adjuvants which are specific to
this form (lubricants, for example) and are liable on the
contrary to produce a flocculating or agglutinating effect.

Moreover, the compression itself produces by
10 definition an agglomeration of the particles which, after
disintegration, no longer redisperse in a unitary state.
Even in the event of "flash disintegration", it proves
difficult to maintain integrity of the initial particle-
size distribution of a substance in tablet form. For
15 various reasons (concealment of taste, protection, spread-
out or delayed action), it is sometimes necessary to coat
the particles of the active ingredient or to fix them on a
support or vehicle of the resin type. The method in
accordance with the invention makes it possible to maintain
20 the integrity of the above-mentioned coating or fixation
of particles which are too fragile in the majority of
instances to withstand the mechanical effects of compression.

Finally, the mixtures to be compressed must have
particular characteristics of "compressibility" which are
25 usually conferred artificially. When the unitary dose is
of high value and the active ingredient has poor

characteristics of compressibility, it is difficult to produce flash-disintegration tablets since the granulation and binding agents which are necessary in order to improve these characteristics can only have the effect of retarding the rate of disintegration.

A further advantage of the lyophilized emulsion in accordance with the invention lies in both qualitative and quantitative broadening of the range of suitable adjuvants for achieving enhanced bioavailability and tolerance.

Thus it is possible in accordance with the invention to incorporate active ingredients provided in the form of fluid, soft, dry, waxy extracts of either animal or vegetable origin and if necessary agents for increasing bioavailability such as, for example,

- natural or synthetic phospholipids which are employed for the formation of liposomes,
- factors of passage and diffusion of medicinal substances (especially alphachymotrypsin, hyaluronidase, etc...)
- and/or products which are capable of reducing the viscosity of the active ingredients and of improving cell-capillary exchanges.

While the size and conditions of manufacture of the tablets and other galenic forms such as soft capsules or gelatine coated capsules able to contain lipid excipients and consequently active ingredients which are partially or totally _____

soluble therein have the effect of limiting the quantity and nature of the adjuvants which can be employed for these galenic forms, the form in accordance with the invention is not subject to any of these restrictions
5 since it can be made from a very wide variety of active ingredients irrespective of the value of their unitary dose. Finally, it should be pointed out that, in the case of utilization of fragile or highly reactive active ingredients, the granulation which is necessary for manu-
10 facture of the tablets is liable to produce changes or incompatibilities. Now it has been found that cold-state manufacture of the novel forms in accordance with the invention removes this drawback since the rate of any possible reactions and degradations is negligible at low
15 temperatures.

* *

It is also known that the following patent specifications : US-A-4 178,695, GB-A-1 227,744, GB-A-1 310,824 and GB-A-1 328,641 have already proposed methods of preparation of pharmaceutical, dietetic or
20 cosmetic forms by lyophilization of at least one active ingredient in solution or suspension in water or an organic solvent or else in an emulsion of the oil-in-water type. The solution proposed in accordance with the invention is distinguished from the technical solutions of the prior
25 art by the operating modes employed. By virtue of these operating modes, the end product is endowed with unexpected

properties, especially in regard to preservation of the active ingredients and in regard to disintegration.

In accordance with the invention, the method for preparing a galenic form for oral administration by lyophilization of an oil-in-water emulsion containing at least one pharmaceutically active ingredient essentially comprises :

- a) preparing the lipid phase by stirring at a temperature lower than or equal to 80°C so as to mix all the lipid-phase components, whereby said lipid phase is liquid,
- b) preparing the aqueous phase, which comprises at least one substance selected from the group consisting of organic fillers and thickening agents, by stirring at a temperature lower than or equal to 80°C so as to mix the water and the other components of said aqueous phase,
- c) preparing an emulsion under stirring at a temperature within the range of 10°C to 80°C by introducing the liquid lipid phase into the aqueous phase in order to obtain a homogeneous emulsion,
- d) distributing the resultant mixture into alveolar packs,
- e) freezing the contents of said alveolar packs at a temperature within the range of -20°C to -50°C , then lyophilizing said contents under a pressure within the approximate range of 6×10^{-1} to 10^{-3} mmHg (that is, between approximately 80 and approximately 0.13 Pa)

with a heat supply such that the temperature of the treated mass is always lower than the starting melting temperature of said mass,

the pharmaceutically active substance being incorporated
5 prior to step d), that is to say either at the time of preparation of the lipid phase of step a) or at the time of preparation of the aqueous phase of step b) or in the homogeneous emulsion obtained in step c) or else at low temperature (between -5°C and -1°C) after step c) but
10 prior to distribution in alveolar packs of step d).

In this specification, the expression "pharmaceutically active substance" is understood to refer to any therapeutically effective ingredient or any association of at least two therapeutically effective ingredients in
15 which said ingredients are either isolated (for example : an active ingredient present in the lipid phase and a second active ingredient present in the aqueous phase, or else an encapsulated or coated active ingredient and a second active ingredient present in either of the two
20 phases) or else intimately mixed.

The essential lipid component contained in the lipid phase consists of at least one substance selected from the group comprising the C_6 - C_{20} -fatty acids, the C_6 - C_{30} - fatty alcohols , the derivatives of said fatty
25 acids, the derivatives of said fatty alcohols, the fats of animal, vegetable and synthetic origin and mixtures of the

thereof . Among the fatty acid derivatives which are suitable for use in accordance with the invention, special mention can be made of the esters and in particular (1) the triglycerides of (C_8-C_{18}) fatty acids obtained from the caprylic, capric, myristic, oleic, linoleic, stearic acids and their mixtures (especially the triglycerides of the acids of the C_8-C_{10} fraction extracted from coconut oil), and (2) the glycerides of saturated ($C_{12}-C_{18}$) fatty acids (which are polyoxyethylenated . Among the fatty alcohol derivatives can be mentioned in particular the esters. Worthy of note among the fats of animal, vegetable and synthetic origin are the oils and the waxes such as, in particular, hydrogenated castor oil, cotton oil, sesame oil, soybean oil, peanut oil, halibut oil, beeswax, the ketowaxes (condensates of alkylene oxides - ethylene and/or propylene oxides - with saturated fatty alcohols) and their mixtures.

If necessary, the lipid phase can contain in addition one or several surface-active agents (preferably non-ionic surfactants) and/or one or several essences.

In practical terms, if no account is taken of the weight of pharmaceutically active substance or of a fraction of this latter to be incorporated if necessary in step a), the essential component as defined in the foregoing can represent approximately 60 to 100 % by weight

with respect to the weight of the lipid phase. Nevertheless, there are cases in which said essential component can represent quantities which are distinctly smaller than 60 % by weight with respect to the weight of said lipid
5 phase.

The aqueous phase which constitutes the continuous phase of the emulsion to be prepared in accordance with the invention comprises an essential component, namely a substance selected from the group of organic
10 fillers, thickening agents and their mixtures.

In practice, it is not easy to make a distinction between organic fillers and thickening agents inasmuch as it is possible in general to find substances which may belong to both categories. For the sake of
15 simplicity, the term "organic fillers" is used in this specification to designate essentially water-soluble substances having a relatively low molecular weight and the term "thickening agents" is used to designate substances which are water-soluble, water-dispersible or capable of
20 being readily dispersed in water and having binding properties or swelling properties in water as well as a higher molecular weight than the organic fillers.

The organic fillers which are suited for use in accordance with the invention include in particular
25 lactose, whole milk powder, semi-skimmed milk powder, skimmed milk powder, glycocoll, mannitol, the maltodextrins

and their mixtures. Suitable thickening agents which are worthy of mention include the polysaccharides such as in particular the natural gums (gum arabic, gum tragacanth, etc.) and the synthetic gums (glycosylglucans in

5 accordance with U.S. patents No 3,507,290 and No 3,659,015), the cellulose derivatives, the pectins, the bentonites, the colloidal silicas, polyvinyl alcohol (PVA), polyvinylpyrrolidone (PVP), the acrylic polymers and copolymers, and the mixtures thereof.

10 In practice, if no account is taken of the weight of the pharmaceutically active substance or a fraction of said active substance to be incorporated if necessary in step b), the group comprising organic filler and thickening means represents approximately 10 to 85 %
15 by weight and advantageously 15 to 65 % by weight with respect to the weight of the aqueous phase of step b).

The group comprising organic filler and thickening means takes part in the formation of the matrix. In broad terms, it may be stated that the organic filler
20 forms the matrix proper and the thickening agent cooperates in the achievement of cohesion and dimensional stability of the matrix. Moreover, the group comprising organic filler and thickening agent performs a contributory function in the adsorption of volatile substances and in
25 the formation of the porous structure of the end product and consequently plays an important part in the release of

the pharmaceutically active substance. It is also possible to improve the bioavailability by employing microgranules of active ingredients coated with a thin gastroresistant envelope.

- 5 Among the dispersing means which can be incorporated in the aqueous phase in step b) or in the lipid phase in step a), recourse can be had to known substances which are suitable for this purpose in the galenic field. Particularly suitable are the non-ionic, anionic and
- 10 cationic surface-active agents. Thus in step b), it is possible to incorporate one or several surface-active agents selected from the following :
- the non-ionic surface-active agents such as the polyoxyethylenated polysorbates or esters of sorbitan
 - 15 (marketed under the trade name of "Tween"^{aa}), the sorbitan esters (marketed under the trade name of "Span"), the copolymers of ethylene oxide and of propylene oxide, the fatty polyethoxyethers of glycerides (especially polyethoxylated castor oil), the cetyl ethers of polyoxy-
 - 20 ethyleneglycol, the palmitostearates of polyoxyethylene-glycol, the soybean and egg lecithins and the like ;
 - the anionic surface-active agents such as in particular^{tt} the (C₄-C₁₂)-dialkyl-sulfosuccinates, especially sodium dioctylsulfosuccinate ;
 - 25 - the cationic surface-active agents such as in particular the quaternary ammonium compounds.

As indicated earlier, these surface-active agents can also be introduced in step a) at the time of preparation of the lipid phase, particularly in the case of the non-ionic surface-active agents.

5 In summary, while it is possible to employ one or a number of surface-active agents in each of the lipid and aqueous phases, it is essential in accordance with the invention to ensure that at least one of these two phases contains a surface-active agent. Advantageously,
10 if no account is taken of the weight of the pharmaceutically active substance or of that fraction of this latter which is to be incorporated in step a) and/or in step b), the quantity of surface-active agent to be employed represents approximately 0.2 % to 10 % by weight and preferably
15 0.4 % to 8 % by weight with respect to the total weight of the lipid and aqueous phases.

Other substances which may be employed in step b) include (1) the natural or synthetic sweetening agents such as saccharose, glucose, xylose, sorbitol, saccharin,
20 the saccharinates (especially the sodium, potassium and calcium saccharinates), the cyclamates (especially the sodium, potassium and calcium cyclamates), aspartame, and (2) taste-modifying agents (in particular for the purpose of concealing the bitter after-taste of synthetic
25 sweeteners of the saccharinate or cyclamate type) such as in particular the citric, ascorbic and tartaric acids, and

aromas.

If so required, it is also possible to incorporate amino-acids in the aqueous phase of step b).

The quantity of water employed in step b) is not
5 critical. Generally speaking, this quantity is limited to the amount which is strictly necessary in order to dissolve and/or disperse the components of the aqueous phase, to produce the emulsion of step c) and to limit the power consumption costs required for carrying out step e). It
10 will readily be understood that, if the ingredients employed in step b) are liquid substances, the water content may be considerably reduced. The water to be employed is a purified water and especially distilled, bi-distilled or demineralized water.

15 The emulsion of step c) is produced in accordance with the invention by stirring at a temperature within the range of 10°C to 80°C by pouring the liquid lipidic phase into the aqueous phase. This operation is advantageously performed at a temperature within the range
20 of 15°C to 60°C. Although it has proved necessary to heat the lipid and aqueous phases in steps a) and b), it may be found advantageous to allow said phases to cool before pouring the lipid phase which is still in the liquid state into the aqueous phase. In practice, the two phases are
25 in accordance with the invention at the same temperature when one phase is poured into the other. Nevertheless,

it may be useful in certain particular instances to provide a temperature gradient by pouring the lipid phase into the aqueous phase at a lipid-phase temperature which is lower than that of said aqueous phase.

5 In a preferred mode of execution of the invention, the emulsion of step c) is prepared in such a manner as to ensure that the weight of the pharmaceutically active substance which may be present is not taken into account and that the weight ratio of lipid phase to
10 aqueous phase is within the range of 1:100 to 1:4 and preferably within the range of 1:50 to 1:6.

Advantageously, the duration of step e) is at least eight hours. The freezing time (which depends on the desired temperature within the range of -20°C to -50°C)
15 is at least one hour on an average in order to obtain by means of a plate-type industrial freezer an identical internal temperature of each of the masses which are distributed within the alveolar packs. The drying time is at least seven hours, taking into account the fact that
20 provision is made in accordance with the invention for a progressive heat supply.

In a preferred embodiment of the method in accordance with the invention, the very fine state of the globules of the emulsion obtained in step c) is maintained
25 intact by means of the following recommended procedure :
1) the homogeneous emulsion obtained in step c) is cooled

by stirring to a temperature below 0°C but preferably within the range of -1°C to -5°C and better still within the range of -2°C to -4°C by introducing it into a scraped-surface exchanger in order to obtain a frozen
5 emulsion ;

- 2) the frozen emulsion thus obtained is distributed in alveolar packs in step d) ;
- 3) the freezing and drying operation is then performed in accordance with step e), the total freezing and drying
10 time being at least eight hours.

As indicated in the foregoing, the pharmaceutically active substance is introduced if necessary in fractions from step a) until initiation of step d). If an active ingredient is sensitive to water, it is introduced
15 into the lipid phase during step a). If there are two active ingredients which are liable to be incompatible with each other prior to administration, they are incorporated separately, one in the lipid phase and the other in the aqueous phase. Advantageously, the
20 incorporation of one of the active ingredients constituting the pharmaceutically active mass is recommended after step c) prior to commencement of step d). As will readily be understood, the pharmaceutically active substance can be introduced in fractions in step a), in step b), in
25 step c) and/or prior to commencement of step d) after execution of step c).

In the case of active ingredients which are particularly sensitive in particular to heat, it is recommended in accordance with a preferred embodiment or mode of application of the invention to introduce said ingredients in a pre-cooled state into the aforementioned frozen emulsion while stirring at a temperature below 0°C but preferably within the range of -1°C to -5°C and better still within the range of -2°C to -4°C, then to distribute the resultant mixture within alveolar packs and then to carry out freezing and drying.

It will of course be apparent that, if necessary, the operations involving introduction of the pharmaceutically active substance and described in the foregoing can be carried out with one or a number of active ingredients in the form of coated granules.

The galenic form obtained in accordance with the invention is porous, lightweight and stable while retaining its initial geometry. The geometrical shape is defined by the mold or so-called alveolar pack in which the product has been distributed. Thus the geometrical shape can be hemispherical, ovoid, cubic, parallelepipedal, conical, frusto-conical, pyramidal, cylindrical, and so on.

The results of tests which have been undertaken show that the method in accordance with the invention retains the initial properties or the properties developed during preparation of the pharmaceutically active

substance, prevents phenomena of recrystallization and polymorphism, prevents denaturation of the fragile active ingredients, and offers the further advantage of stabilizing the partition coefficient of the active ingredients of the pharmaceutically active substance between the dispersed oily phase and the continuous aqueous phase, which is liable to vary in particular when there is a variation in parameters such as temperature.

The galenic form in accordance with the invention can be administered with or without water. It can be taken by placing it under the tongue, crunching between the teeth or allowing it to disintegrate in the mouth. A liquid emulsion can also be obtained extemporaneously by dispersing it in water.

Other advantages and features of the invention will be more apparent from a perusal of the following examples of preparation which are given solely by way of explanatory illustration and not in any limiting sense.

Example 1

Tiadenol at 1200 mg

Unitary formula :

A	Tiadenol	1200 mg
	Triglyceride of caprylic and capric acids	200 mg
B	Polysorbate 60	20 mg
	Polyethoxyether of fatty glycerides	20 mg

C	[Sodium saccharinate	10 mg
		Dextran 70 000	50 mg
		Lactose	300 mg
		Demineralized water	1400 mg

5 Manufacturing technique :

1. Mix and heat the ingredients of the lipid phase B at 65°C.
2. Dissolve and disperse the elements of the aqueous phase C and heat said phase to 65°C.
- 10 3. Pour B into C while stirring, continue the stirring operation and allow to cool to 45°C.
4. Add the active ingredient A to the emulsion B + C at 45°C and homogenize by means of a rapid disperser in order to obtain a fine and stable emulsion.
- 15 5. Distribute the emulsion thus obtained into alveolar packs in a proportion of 3.20 ± 0.05 g per alveolar pack.
6. The alveolar packs are driven to low temperature on the plates of a lyophilizer. Allow the temperature to
20 attain equilibrium at -35°C over a period of one hour and begin the lyophilization process by production of a vacuum within the vessel (approximately 10^{-1} mmHg, namely approximately 13.3 Pa) and by heating the plates on which the alveolar packs are placed. The
25 drying process takes place progressively with a supply of heat such that the temperature of the mass

-20-

is necessarily maintained below its starting melting point. The length of the freezing-drying cycle is approximately 10 to 12 hours.

In accordance with this technique, the fragments thus obtained have a uniform shape, a porous state, a unitary weight of 1800 ± 50 mg and each containing approximately 1200 mg of tiadenol. These alveolar packs containing said fragments are heat-sealed with sheets of aluminum/PVC complex and packaged.

10 Example 2

Erythromycin at 1000 mg

15	B	A Erythromycin ethylsuccinate (in a sufficient quantity for 1000 mg of base)	1175 mg
		Triglyceride of caprylic, capric and linoleic acids	250 mg
		Soybean lecithin	20 mg
20	C	Copolymer of polyoxyethylene, of polyoxypropylene and of propyleneglycol	60 mg
		Sodium saccharinate	10 mg
		Hydroxypropylmethylcellulose	10 mg
		Powdered, semi-skimmed milk	300 mg
		Ammonium glycyrrhizinate	5 mg
		Bidistilled water	2000 mg

The process is performed as in Example 1 by introducing the active ingredient A into the emulsion B + C at a temperature below 20°C and by distributing into

each alveolar pack 3.83 ± 0.05 g of the resultant emulsion.

Example 3

Glafenin at 200 mg

5	A	Glafenin	200 mg
	B	Hydrogenated and stripped (C_8-C_{12}) coconut oil	50 mg
		Soybean lecithin	10 mg
10	C	Sodium dioctylsulfosuccinate	10 mg
		Sodium saccharinate	5 mg
		Aspartame	20 mg
		Powdered whole milk	150 mg
		Mannitol	500 mg
		Demineralized water	1000 mg

The process is performed as in Example 1 by introducing the active ingredient A at $15 - 20^\circ C$ in the emulsion B + C and by distributing within each alveolar pack 1.945 ± 0.050 g of the resultant emulsion.

Example 4

Glafenin at 150 mg

20	A	Glafenin	150 mg
	B	Polyoxyethylenated oleic glycerides	50 mg
		Sorbitan monostearate	10 mg
		Polyoxyethylene monostearate	10 mg
25	C	Saccharin	10 mg
		Lactose	500 mg
		Saccharose monopalmitate	1 mg
		Distilled water	1000 mg

The process is performed as in Example 3.

Example 5

Floctafenin at 200 mg

	A	Floctafenin	200 mg
5	B	[Hydrogenated castor oil	100 mg
		Polysorbate 60	10 mg
		Sorbitan monooleate	10 mg
10	C	[Sodium saccharinate	10 mg
		Hydroxypropylmethylcellulose	5 mg
		Mannitol	500 mg
		Demineralized water	1000 mg

Preparation at 60°C for each phase B and C and addition of A to B + C at 60°C, followed by treatment in accordance with the process described in Example 1.

Example 6

Micronized spironolactone at 50 mg

15	A	Micronized spironolactone	50 mg
	B	Triglycerides of capric and caprylic acids	25 mg
		Soybean lecithin	5 mg
20	C	Saccharose monopalmitate	0.5 mg
		Powdered whole milk	100 mg
		Lactose	300 mg
		Purified water	700 mg

The process is performed as in Example 1 by introducing A in the emulsion B + C at 20°C.

Example 7

Indometacin at 75 mg

25	A	Indometacin	75 mg
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B	[Polyoxyethylenated oleolinoleic glycerides	50 mg
		Polyoxyethylene(2)cetyl ether	10 g
		Polyoxyethylene(10)cetyl ether	10 mg
5 C	[Saccharose distearate	5 mg
		Powdered whole milk	100 mg
		Lactose	300 mg
		Distilled water	700 mg

The process is performed as in Example 1 in order to prepare the emulsion B + C. This emulsion is then introduced into a scraped-surface exchanger and cooled. When the temperature attains -2°C , the active ingredient A which has previously been cooled to -2°C is introduced and stirring is continued in order to obtain a homogeneous "frozen emulsion". The cold emulsion is distributed in alveolar packs, whereupon freezing and drying are carried out as in Example 1.

Example 8

Naproxene at 250 mg

A	Naproxene	250 mg	
.20	[Olive oil	80 mg
		Polysorbate 60	15 mg
		Sorbitan monostearate	15 mg
C	[Glycyrrhizine	7 mg
		Aspartame	15 mg
		Mannitol	500 mg
		Distilled water	1200 mg
25			

D	[Coconut aroma	50 mg
	[Anise aroma	5 mg

The process is performed as in Example 1 by preparing the phases B and C at 65°C and by introducing 5 A and D in the emulsion B + C at 40°C.

Example 9

Vitamin complex

10	A	[Vitamin A palmitate	2.3 mg
		[D,L- α -tocopherol acetate	10 mg
		[Calciferol (D3)	0.4 mg
		[Polysorbate 80	20 mg
15	B	[Mandarin oil	20 mg
		[Thiamine mononitrate	2 mg
		[Riboflavin	2 mg
		[Calcium pantothenate	9.3 mg
		[Pyridoxine hydrochloride	1 mg
20	B	[Nicotinamide	15 mg
		[Ginseng (extract)	40 mg
		[Saccharose	25 mg
		[Polymer of ethylene oxide	
		[Propylene oxide and propyleneglycol	50 mg
C		[Sodium saccharinate	13 mg
		[Lactose	700 mg
		[Demineralized water	1000 mg
	C	Ascorbic acid coated with ethylcellulose	60 mg

1. Dissolve the mixture A.
2. Disperse the mixture B.
3. Mix A with B while stirring, and homogenize.
4. Pass the emulsion obtained in a scraped-surface
- 5 exchanger and cool to a temperature of approximately
-2°C to -3°C, add C, then homogenize.
5. Proceed as indicated in Example 7 for distribution in
alveolar packs, freezing and drying.

Example 10 Buflomedil hydrochloride at 150 mg

10	A	Buflomedil hydrochloride	150 mg
		Cation - exchange resin	170 mg
	B	Triglyceride of caprylic and capric acids	50 mg
		Polysorbate 60	5 mg
		Polyethoxyether of fatty glycerides	5 mg
15	C	Sodium saccharinate	15 mg
		Aspartame	15 mg
		Dextran 70 000	40 mg
		Mannitol	527 mg
		Orange oil	16 mg
20		Aluminum and magnesium silicate	7 mg
		Demineralized water	1000 mg

The process is performed as in the foregoing
 Example 7. A kinetic study on dogs clearly points to the
 fact that the product obtained in accordance with
 25 Example 10 effectively releases in vivo the buflomedil

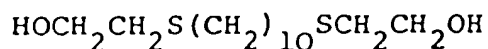
hydrochloride adsorbed on the cation-exchange resin.

COMPARATIVE TESTS

The summary given below describes part of the comparative tests which have been carried out with the novel oral forms in accordance with the invention.

TEST I

For the purpose of comparison, the product obtained in accordance with the foregoing Example 1 containing 1200 mg of tiadenol and the commercial specialty known as "Fonlipol" (three tablets each containing 400 mg of tiadenol) were administered clinically to patients suffering from hyperlipemia (group of eight male adults per product to be tested by oral administration, each patient receiving the same dose (1200 mg) of tiadenol. It is recalled that tiadenol, which has the following developed formula :



and corresponds to the systematic nomenclature of 1,10-bis(2-hydroxyethylthio)decane, is a reference lipid reducing agent described in particular in DE-A-2,038,836.

There were then determined the serum concentrations of tiadenol (mg/l) as a function of time (hr). The results have been recorded in Fig. 1, in which curve 1 relating to the product of Example 1 has been plotted from minimum values of the confidence interval and in which

curve 2 relating to the compressed tablet form previously known has been plotted from maximum values of the confidence interval.

A comparison of Figs. 1 and 2 reveals the fact that the latency period after administration of the product of Example 1 is considerably reduced with respect to the tablets. There is also observed a statistically significant difference in regard to the concentrations of tiadenol in the blood by comparing the areas beneath the concentration/ time curves.

TEST II

For the purpose of comparison, an identical dose (150 mg) of buflomedil hydrochloride was administered orally to dogs (distributed in batches of nine animals per batch). From the galenic standpoint, this active ingredient was packaged in three different forms :

- one batch of animals received the product of Example 10 above (A) ;
- one batch of animals received the compressed tablet of buflomedil hydrochloride which is marketed under the trade name of "Fonzylane" (Registered trademark) (cf. in particular Dictionnaire Vidal, O.V.P., Paris 1983, page 525) (B) ; and
- one batch of animals received a tablet in which the active ingredient was associated with 170 mg of the same cation-exchange resin considered in Example 10 (C) .

It has been found that the adsorption resin contained in the product of Example 10 does not prevent the release of the active ingredient in vivo. A kinetic study of bioavailability in vivo shows that the areas
5 beneath the curve of plasmatic concentrations/time are not different in the case of groups A and B and that there exists a statistically significant difference in the case of batches A and B with respect to batch C since batch C gives plasmatic concentrations which are lower than those
10 of batches A and B over the test period considered.

WHAT IS CLAIMED IS :

1. A method for preparing a galenic form for oral administration by lyophilization of an oil-in-water emulsion containing at least one pharmaceutically active ingredient and obtained from a lipid phase and an aqueous phase, wherein said method comprises :
 - a) preparing the lipid phase by stirring at a temperature lower than or equal to 80°C so as to mix all the lipid-phase components, whereby said lipid phase is liquid,
 - 10 b) preparing the aqueous phase, which comprises at least one substance selected from the group consisting of organic fillers and thickening agents, by stirring at a temperature lower than or equal to 80°C so as to mix the water and the other components of said aqueous phase,
 - 15 c) preparing an emulsion under stirring at a temperature within the range of 10°C to 80°C by introducing the liquid lipid phase into the aqueous phase in order to obtain a homogeneous emulsion,
 - 20 d) distributing the resulting mixture into alveolar packs,
 - e) freezing the contents of said alveolar packs at a temperature within the range of -20°C to -50°C , then lyophilizing said contents under a pressure within the approximate range of 80 Pa to 0.13 Pa, with a heat supply such that the temperature of the treated mass is always lower than the starting melting temperature of said mass,
 - 25

the pharmaceutically effective material being incorporated before step d).

2. A method according to claim 1, wherein the pharmaceutically active substance is incorporated from step a) up to the point of commencement of step d), if necessary by fractions.
3. A method according to claim 1, wherein at least a fraction of the pharmaceutically active substance is incorporated in step c).
- 10 4. A method according to claim 1, wherein at least a fraction of the pharmaceutically active substance is incorporated at a temperature below 0°C and preferably within the range of -1°C to -5°C in the homogeneous emulsion resulting from step c).
- 15 5. A method according to claim 1, wherein a surface-active agent is introduced in at least one of steps a) and b).
6. A method according to claim 1, wherein the organic filler of step a) is selected from the group consisting of lactose, whole milk powder, semi-skimmed milk powder, skimmed milk powder, glycocoll, mannitol, the maltodextrins, and the mixtures thereof.
- 20 7. A method according to claim 1, wherein the thickening agent is selected from the group consisting of the natural and synthetic gums, the cellulose derivatives, 25 the pectins, the bentonites, the colloidal silicas,

polyvinyl alcohol, polyvinylpyrrolidone, the acrylic polymers and copolymers, and the mixtures thereof.

8. A method according to claim 1 wherein, if the weight of the pharmaceutically active substance which may be present in step b) is not taken into account, the group consisting of organic filler and thickening agent represents approximately 10 to 85 % by weight and advantageously 15 to 65 % by weight with respect to the weight of the aqueous phase.

9. A method according to claim 1 wherein, if the weight of the pharmaceutically active substance which may be present in steps a) and b) is not taken into account, the emulsion of step c) is prepared in such a manner as to ensure that the weight ratio of lipid phase to aqueous phase is within the range of 1:100 to 1:4 and preferably within the range of 1:50 to 1:6.

10. A method according to claim 5 wherein, if the weight of the pharmaceutically active substance which may be present in steps a) and b) is not taken into account, the surface-active agent represents approximately 0.2 % to 10 % by weight and preferably 0.4 % to 8 % by weight with respect to the total weight of the lipid and aqueous phases.

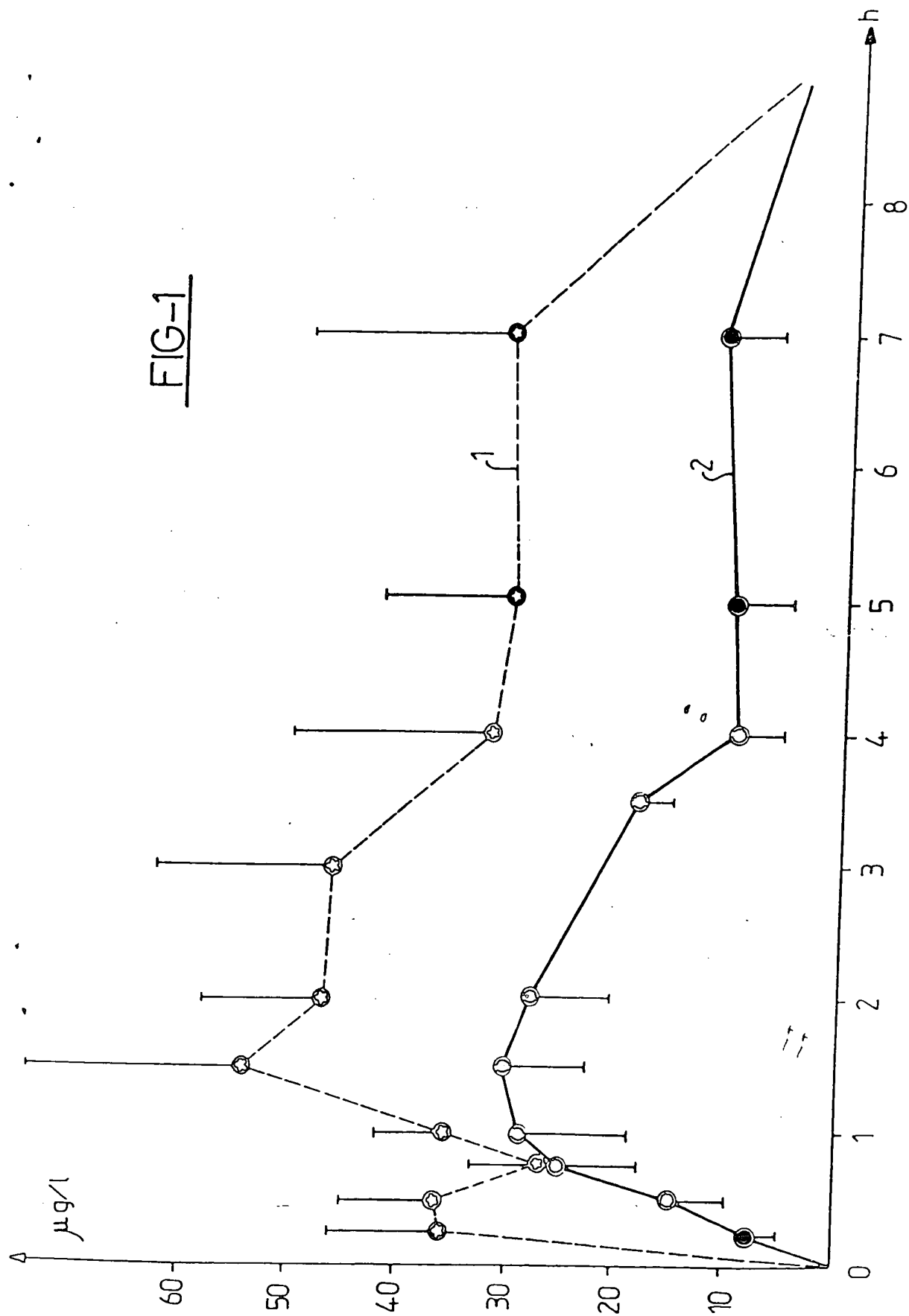
11. A method according to claim 1, wherein the duration of step e) is at least eight hours, the freezing time at a temperature within the range of -20°C to -50°C

being at least one hour on an average, a progressive heat supply being provided during the drying process.

12. A method according to claim 1 wherein, after step c), the homogeneous emulsion obtained in said step c)
5 is cooled by stirring to a temperature below 0°C and preferably within the range of -1°C to -5°C in order to obtain a frozen emulsion which is then subjected to steps d) and e).

13. A porous galenic form, which is
10 obtained by means of the method according to claim 1.

FIG-1



DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.4)
X,Y	GB-A- 806 723 (ICI) * Whole document *	1-13	A 61 K 9/10 A 61 K 9/14
D,Y	GB-A-1 328 641 (ORSYMONDE) * Whole document *	1-13	
Y	DE-A-2 017 373 (ORSYMONDE) * Whole document *	1-13	
A	CHEMICAL ABSTRACTS, vol. 88, no. 6, 6th February 1978, page 254, no. 41696s, Columbus, Ohio, US; & JP - A - 77 125 615 (KYOWA HAKKO KOGYO CO., LTD.) 21-10-1977		
A	CHEMICAL ABSTRACTS, vol. 68, 1968, page 9544, no. 98627m, Columbus, Ohio, US; MANUEL LLADSER PRADO: "Lyophilization of oil-in-water emulsion" & AN. FAC. QUIM. FARM., UNIV. CHILE 18, 163-71		TECHNICAL FIELDS SEARCHED (Int. Cl.4) A 61 K
A	CHEMICAL ABSTRACTS, vol. 87, no. 16, 17th October 1977, page 323, no. 122707c, Columbus, Ohio, US; DEVRAJ RAMBHAU et al.: "Stability studies on lyophilized o/w emulsions" & INDIAN J. PHARM. 1977, 39(3), 52-5		
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 05-07-1985	Examiner BENZ K. F.
<p>CATEGORY OF CITED DOCUMENTS</p> <p>X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document</p> <p>T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons</p> <p>& : member of the same patent family, corresponding document</p>			



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Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.4)
A	CHEMICAL ABSTRACTS, vol. 91, no. 3, 16th July 1979, page 497, no. 18602m, Columbus, Ohio, US; FREDERIK GEJL-HANSEN et al.: "Microstructure of freeze dried emulsions: effect of emulsion composition" & J. FOOD PROCESS. PRESERV. 1979, 2(3), 205-28 -----		
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